

Vapor Recovery Tower

1.1 Quote Information

Customer Information											
Name						Compa	ny				
Business Title											
Email					Phone Numbe						
	Equipment Information										
Quantity				Ship to Locatio (City, State, Zip							
Proposal Due Date			_	Freight ☐ EXW ☐ FCA ☐ FOB ☐ CIF Terms ☐ Other							
Potential Order Da		:				Preferre Ship Da					
Rank (1-4) Importance of the Following:											
Price:			Spec Compliance:			Delivery:			Quality/Reliability:		
Additional Comments											

1.2 Process Conditions

Process Data	Parameter	VRT
Inlet Pressure (PSIG)		Atmos.
Inlet Temp (°F)		70 - 120
Design Pressure (PSIG)		75-125
Gas Inlet Flowrate (MMSCFD)		< 0.5
Oil Inlet Flowrate (BBL/Day)		1000-6000
Oil Inlet SG / API		0.7
Fluid Elevation in Tank or NPSHA (Ft)		20-30
Retention Time (min)		20-25
Inlet Fluid Composition		
Shon Canabla Siza	<60"OD, <40'S/S, <125#	Required
Shop Capable Size		Requested

Revision 2 © Cimarron Energy, 16Jun2020 Page 1	on 2 © Cimarron Energy, 16.	Jun2020 Page 1
--	-----------------------------	----------------



1.3 Design Scope

☐ 30ft ☐ 35ft ☐ 40ft ☐ Other	
MAWP:	
☐ 75 psig ☐ 100 psig ☐ 125 psig [☐ Other
□ Bare Vessel	
□ Vessel with Accessories	
Outlet Piping	
☐ Cimarron Standard SP-3/DTM 1	Coat, Color: Desert Tan
☐ Cimarron Standard SP-6/2 Coa	t, Color: Desert Tan
□ Custom	
Accessories (Ship Loose	of Bare Vessel option)
Item:	OEM/Type Preference:
☐ Concrete Blocks	
□ PSV	
Gauges (Level, PI, TI)	
☐ Sight	
□ Transmitters	
Additional Requests	
	MAWP: 75 psig 100 psig 125 psig Bare Vessel Vessel with Accessories Outlet Piping Cimarron Standard SP-3/DTM 1 Cimarron Standard SP-6/2 Coa Custom Accessories (Ship Loose Item: Concrete Blocks PSV Gauges (Level, PI, TI) Sight



1.4 Application Guidance

A Vapor Recovery Tower technically meets the standards of being a pressure vessel and thus is considered by the EPA to be process equipment. It is not considered to be a storage tank and is not subject to the Quad O Regulations.

- Pressure vessels designed to operate in excess of 204.9 kilopascals and without emissions to the atmosphere are exempt.
- Although VRT's are normally rated for pressures between 50 and 175 psig, they typically gravity
 feed to the liquid storage tanks at very low pressure (~1 psig) In most installations, the flash
 gas from the liquids in the VRT flow to a vapor recovery unit for compression
- The area above the normal liquid level is used as a vapor space and a VRU is used to maintain a pressure of ~1 psig ♣ Liquid should have a retention time of approximately 25-30 minutes

How does a VRT work? Benefits of Vapor Recovery

- Vapor Recovery Towers isolate liquid storage tanks from the pressures associated with the oil vapors
- Vapor Recovery Towers can help keep some facilities from falling under the requirements of the New Source Performance Standard ("Quad O")
- Vapor Recovery Towers help keep air (and therefore, oxygen) out of gas pipelines by sequestering the vapors in the Tower and eliminating the vapor containment potential common to atmospheric tanks
- The VRT serves as the last designated pressure vessel to collect vapors off of the oil and send them to the VRU / flare / combustor without the propensity to leak that storage tanks typically have.

1.5 Sizing Information

Parameter					Data				
Tower OD (inches)	24	24	36	36	48	48	60	60	60
Tower S/S Height (ft)	30	40	30	40	30	40	30	40	40
Liquid Outlet from Bottom Head Seam (ft)	27	37	25.5	35.5	24	34	22.5	32.5	32.5
Liquid Outlet Downcomer from Bottom Head seam (ft)	2	2	2	2	2	2	2	2	2
Volume Barrels	14	19.6	29.6	42.2	49.2	71.6	71.7	107	107
BBL Fluid per day Max @ 20 Minutes	1007	1410	2130	3037	3545	5157	5162	7680	7680
BBL Fluid per day Max @ 25 Minutes	806	1128	1704	2429	2836	4125	4129	6144	6144
BBL Fluid per day Max @ 30 Minutes	671	940	1420	2024	2364	3438	3441	5120	5120

	Revision 2	© Cimarron Energy, 16Jun2020	Page 3
--	------------	------------------------------	--------